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7. (Amended) A process according to claim 34, wherein at least 90% of the C<sub>2</sub> to C<sub>3</sub> compounds present in the effluent are present as C<sub>2</sub> to C<sub>3</sub> olefins.

8. (Amended) A process according to claim 35, wherein at least 95% of C<sub>2</sub> to C<sub>3</sub> compounds present in the effluent are present as C<sub>2</sub> to C<sub>3</sub> olefins.

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20. (Amended) A process for the cracking of olefins in a hydrocarbon feedstock containing at least one diene and at least one olefin, the process comprising hydrogenating the at least one diene to form at least one olefin in the presence of a transition metal-based hydrogenation catalyst at an inlet temperature of from 40 to 200°C and an absolute pressure of from 5 to 50 bar with a hydrogen/diene molar ratio of at least around 1, and catalytically cracking the olefins in the presence of a crystalline silicate catalyst having a silicon/aluminum atomic ratio of from 180 to 1000 at an inlet temperature of from 500 to 600°C and an olefin partial pressure of from 0.1 to 2 bar to produce at least one olefin having a different olefin distribution with respect to average carbon number than the at least one olefin in the feedstock. (112)

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27. (Amended) A process for the catalyst cracking of olefins to lighter olefins, the process comprising contacting a first hydrocarbon stream comprising light cracked naphtha and a second hydrocarbon stream comprising C<sub>4</sub> olefins with a crystalline silicate catalyst having a silicon/aluminum atomic ratio of from 180 to 1000 at a temperature of from 500 to 600°C and at an absolute pressure of from 0.5 to 2 bars to produce an effluent stream rich in lighter olefins.

Please add the following new claims.

34. A process for cracking an olefin-rich hydrocarbon feedstock which is selective towards propylene in the effluent, the process comprising contacting a hydrocarbon feedstock containing olefins having a first composition of at least one olefinic component with a crystalline silicate catalyst having a silicon/aluminum atomic ratio of from 180 to 1000 to produce an effluent having a second composition of at least one olefinic component, the feedstock contacting the catalyst at an inlet temperature of from 500 to 600°C and being passed over the catalyst at an LHSV of from 10 to 30h<sup>-1</sup>, the feedstock and the effluent having substantially the same olefinic content by weight therein, and the effluent having a higher propylene content than the feedstock, wherein the feedstock comprises a light cracked naphtha.

35. A process for cracking an olefin-rich hydrocarbon feedstock which is selective towards propylene in the effluent, the process comprising contacting a hydrocarbon feedstock containing olefins having a first composition of at least one olefinic component with a crystalline silicate catalyst having a silicon/aluminum atomic ratio of from 180 to 1000 to produce an effluent having a second composition of at least one olefinic component, the feedstock contacting the catalyst at an inlet temperature of from 500 to 600°C and being passed over the catalyst at an LHSV of from 10 to 30h<sup>-1</sup>, the feedstock and the effluent having substantially the same olefinic content by weight therein, and the effluent having a higher propylene content than the feedstock, wherein the feedstock is selected from the group consisting of a C<sub>4</sub> cut from a fluidised-bed catalytic cracking unit in a refinery, or a C<sub>4</sub> cut from a unit in a refinery for producing methyl tert-butyl ether and a C<sub>4</sub> cut from a steam-cracking unit.